## Journal of Chromatography, 76 (1973) 221-228

() Elsevier Scientific Publishing Company, Amsterdam --- Printed in The Netherlands

# снком. 6424

# ION-EXCHANGE PROCESSES OF SOME TRIVALENT ELEMENTS ON AMORPHOUS ZIRCONIUM PHOSPHATE UP TO 250°C

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# SUMMARY

The effect of temperature in the range  $25-250^{\circ}$  on the distribution of trace amounts of radioactive Eu<sup>3+</sup>, Ce<sup>3+</sup> and Fe<sup>3+</sup> on amorphous zirconium phosphate, and also the effect of nitric acid concentration, have been studied. The experiments were carried out at 25°, 50°, 110°, 150°, 200° and 250°. With increasing temperature, the distribution of the trace amounts of Eu<sup>3+</sup> and Ce<sup>3+</sup> increased very slightly, while the increase in the distribution of Fe<sup>3+</sup> was greater. Furthermore, it was concluded that the reactions investigated are endothermic.

These distribution data were used for the calculation of the thermodynamic equilibrium constants and other thermodynamic data.

## INTRODUCTION

Zirconium phosphate, which is used as a sorbent to remove the ionic impurities from the cooling water of PWR and BWR reactors<sup>\*</sup>, has become of interest in connection with its ion-exchange, chemical and mechanical properties at high temperatures<sup>1-7</sup>.

In order to continue the study of ion-exchange processes on amorphous zirconium phosphate at high pressure and high temperature, experiments with trace amounts of radioactive  $Ce^{3+}$ ,  $Eu^{3+}$  and  $Fe^{3+}$  in nitric acid solutions were carried out. The effect of temperature in the range 25-250° on the ion-exchange processes was studied as a function of nitric acid concentration.

#### EXPERIMENTAL

# Preparation of zirconium phosphate

Granulated amorphous zirconium phosphate was prepared by the method described by VESELY AND PEKAREK<sup>8</sup>. After drying at 110°, a grain-size fraction of r = 0.04 mm was separated. The P/Zr ratio in the exchanger was 2.02. The capacity of the ion exchanger was found to be 2.40 mequiv. per gram of air-dried zirconium phosphate.

# Procedure.

A 2.5 g amount of amorphous zirconium phosphate was equilibrated in an  $autoclave^5$  in 250 ml of solution. The samples were removed from the autoclave

\* PWR = pressure water reactor; BWR = boiling water reactor.

through a water-cooled stainless-steel tube. The equilibration time was 6 h, which was found to be a sufficient period for equilibrium to be attained.

## Analytical methods

The P/Zr ratio was determined in the zirconium phosphate sample by the method described by VESELY AND PEKAREK<sup>8</sup>. Radiometric determinations were performed by means of a  $\gamma$ -scintillation detector (Nuclear Chicago M-DSS5B, with a NaI (TII) crystal).

The concentration of nitric acid was determined by titration with a standard solution of sodium hydroxide.

All the reagents used were of "pro analysi" grade.

#### RESULTS AND DISCUSSION

The results for two runs which prove the reversibility of the ion-exchange reactions of the trivalent cations studied are presented in Fig. x. In the first run, the trace amounts of radioactive Eu<sup>3+</sup> ions were present in the initial solution, while in the second run they were adsorbed at the start on amorphous zirconium phosphate. It is clear from these two runs that the ion-exchange process studied is reversible.



Fig. 1. Reversibility of  $Eu^{3+}/H^+$  ion-exchange reaction on amorphous zirconium phosphate at 25°. O,  $Eu^{3+}/H^+$  ion-exchange process;  $\bullet$ ,  $H^+/Eu^{3+}$  ion-exchange process.

#### ION EXCHANGE ON ZIRCONIUM PHOSPHATE

In order to study the effect of temperature on the ion-exchange process as a function of the concentration of nitric acid, experiments were carried out in an autoclave. The pressure was maintained constant at So atm and experiments with different acidities in the aqueous phase were carried out at  $25^{\circ}$ ,  $50^{\circ}$ ,  $110^{\circ}$ ,  $150^{\circ}$ ,  $200^{\circ}$  and  $250^{\circ}$ C. The results are shown in Figs. 2-4.



Fig. 2. The exchange of  $Eu^{n+}$  as a function of the nitric acid concentration in the aqueous phase in the temperature range  $25-250^{\circ}$ .

It is obvious from Fig. 2 that the effect of temperature on the distribution of  $Eu^{3+}$  between aqueous nitric acid and zirconium phosphate is very small. This result was also obtained by BAETSLE<sup>9</sup> in the temperature range 25-75°. In our work the effect of temperature on the  $Eu^{3+}/H^+$  ion-exchange process was opposite to that on the  $Cs^+/H^+$  and  $Ca^{2+}/H^+$  ion-exchange processes<sup>6,7</sup>. The distribution coeffcient ( $K_d = n_M/m_M$ , where n is the number of millimoles of an ion per gram of the air-dried exchanger and m is the aqueous molality of ion) for the  $Eu^{3+}/H^+$  ion exchange slowly increases with increasing temperature.

The effect of temperature on the  $Ce^{3+}/H^+$  ion-exchange process is shown in Fig. 3. In this instance the effect of temperature is greater than in the  $Eu^{3+}/H^+$  ion-exchange process.

The effect of temperature on the distribution of Fe<sup>3+</sup> between aqueous nitric



Fig. 3. The exchange of  $Ce^{a+}$  as a function of the nitric acid concentration in the aqueous phase in the temperature range  $25-250^{\circ}$ .

Fig. 4. The exchange of  $Fe^{3+}$  as a function of the nitric acid concentration in the aqueous phase in the temperature range  $25-150^{\circ}$ .

acid and amorphous zirconium phosophate (Fig. 4) is greater than in the  $Eu^{3+}/H^+$  ion-exchange process.

In the study of the  $Fe^{3+}/H^+$  ion-exchange process at temperatures above 150°, extensive hydrolysis of  $Fe^{3+}$  occurred.

The hydrolysis of Fe<sup>3+</sup> at higher temperatures could be an advantage in water purification systems. The product of the hydrolysis is magnetite,  $(Fe_3O_4)^{10}$ , which is removed by means of a micropore filter.

The  $Fe^{3+}/H^+$  ion-exchange process was not studied at temperatures above 150° owing to the extensive hydrolysis. However, the results obtained below 150° also have to be accepted with reserve because of the unknown state of the iron ions under such hydrothermal circumstances.

The exchange of an  $M^{z+}$  ion on the ion exchanger HR in the H<sup>+</sup> form, can be expressed by the equation:

$$M_{(aq)}^{z+} + zHR_{(s)} = MR_{z(s)} + zH_{(aq)}^{+}$$

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where the subscript (aq) denotes the aqueous phase and (s) denotes the solid phase.

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(1)

According to an earlier paper<sup>11</sup>, where  $M^{z+}$  is present at trace concentration, the following equation is obtained:

$$\log K_d = -z \log \left[ m_{\rm H} (\gamma_{\pm \rm HNO_3})^2 (\gamma_{\pm \rm M(NO_3)_z})^{-(z+1)/z} \right] + \log C + \log K \tag{2}$$

where  $\gamma_{\pm}$  is the mean molar activity coefficient and  $C = n_{\rm H}$  is the "unifunctional" capacity of the ion exchanger.

The last two terms in eqn. 2 are constant. Therefore, the graph of log  $K_d$  on the logarithm of the term in the square brackets should be a straight line with a

TABLE I

EQUILIBRIUM CONSTANTS FOR THE  $Eu^{3+}/H^+$  ion-exchange process on amorphous zirconium phosphate at 25°, 50°, 110°, 150°, 200° and 250° calculated by Eqn. 2

Temperature (°C)	2		ĸ	
	Theoretical	Calculated		
25	3	3.4	$(7.25 \pm 2.88) \cdot 10^{-2}$	
50	3	3.3	$(8.75 \pm 5.41) \cdot 10^{-2}$	
110	3	3.4	$(1.03 \pm 0.41) \cdot 10^{-1}$	
150	3	3.3	$(2.09 \pm 1.18(\cdot 10^{-1}$	
200	3	3.3	$(2.49 \pm 1.02) \cdot 10^{-1}$	
250	3	3.4	$(3.57 \pm 1.35) \cdot 10^{-1}$	

#### TABLE II

EQUILIBRIUM CONSTANTS FOR THE  $Ce^{3+}/H^+$  ion-enchange process on amophous zirconium phosphate at 25°, 50°, 110°, 150°, 200° and 250° calculated by Eqn. 2

Temperature (°C)	\$		ĸ	
	Theoretical	Calculated		
25	3	2.8	$(5.81 + 0.51) \cdot 10^{-3}$	
50	3	3.1	$(8.09 \pm 1.25) \cdot 10^{-3}$	
110	3	3.0	$(1.01 \pm 0.04) \cdot 10^{-3}$	
150	3	3.0	$(1.51 \pm 0.07) \cdot 10^{-3}$	
200	3	2.9	$(2.05 \pm 0.09) \cdot 10^{-2}$	
250	3	3.0	$(2.78 \pm 0.11) \cdot 10^{-2}$	

## TABLE III

EQUILIBRIUM CONSTANTS FOR THE  $1^{5}c^{3+}/H^{+}$  ion-enchange process on amorphous zirconium phosphate at 25°, 50°, 110, 150°, 200° and 250° calculated by Eqn. 2

Temperature (°C)	2		ĸ	
	Theoretical	Calculated		
25	3	2.8	$(5.81 \pm 2.62) \cdot 10^{-3}$	
50	3	3.1	$(1.28 \pm 0.68) \cdot 10^{-2}$	
110	3	3.2	$(8.33 \pm 2.06) \cdot 10^{-8}$	
150	3	3.4	$(1.89 \pm 0.64) \cdot 10^{-1}$	

slope z. By determining the value of the slope, z, the equilibrium constant of the observed ion-exchange reaction can be calculated. The values for  $\gamma_{\pm \text{HNO}_s}$  were taken directly from LIETZKE's tables<sup>12</sup>, while the values for  $y_{\pm \text{M(NO}_s)_z}$  were calculated assuming the validity of the Guggenheim's case of HARNED's rule<sup>13</sup>.

From the calculated slopes, which are approximately three, we concluded that the ion-exchange processes studied involve the exchange of three hydrogen ions from zirconium phosphate and one trivalent ion from the solution.

Equilibrium constants calculated by using z = 3 are shown in Tables I-III.

## TABLE IV

calculated thermodynamic values for the  ${\rm Eu}^{a+}/{\rm H}^+$  ion-exchange process on amorphous zirconium phosphate

Temperatu (°C)	ire in K	AH3 (kcal/mole)	AG° (kcal/mole)	⊿S° (cal/mole∙degree)
25		0.65 <sup>8</sup>	1.1.4%	1.67 <sup>n</sup>
25	-2.62	2,20	1.54	2.21
50	-2.43	2.20	1.56	1.98
110	- 2.27	2,20	1.72	1.75
150	T.5Ö	2,20	1.31	2.10
200	- 1.39	2.20	1.30	1,90
250		2.20	1.15	2.01

<sup>a</sup> Values obtained by BAETSLE<sup>9</sup>.

## TABLE V

CALCULATED THERMODYNAMIC VALUES FOR THE  $Ce^{3+}/H^+$  ion-exchange process on amorphous zirconium phosphate

Temperature in K (°C)		∆H° (kcal/mole)	∠lG ° (kcal/mole)	∆S° (cal/mole+degree)
25	- 5.15	2.00	3.04	- 3.48
50	-4.82	2,00	3.10	-3.40
110	-4.58	2.00	3.48	3.87
150	-4.18	2.00	3.50	
200	-3.89	2.00	3.64	- 3.47
250	-3.59	2.00	3.79	- 3.29

#### TABLE VI

Calculated thermodynamic values for the  $Fe^{3+}/H^+$  ion-exchange process on amorphous zirconium phosphate

Temperature (°C)	ln K	∆H° (kcal/mole)	∠1G° (kcal/mole)	⊿1S° (cal/mole•degree)
25	5.22	5.60	3.11	8.39
50	-4.32	5.00	2.78	8.73
110	-2.49	5.60	1.89	9.70
150	- 1.67	5.60	1.40	9.93



Fig. 5. Temperature dependence of the thermodynamic equilibrium constants for  $Eu^{3+}/H^+$  (O)  $Ce^{3+}/H^+$  (O) and  $Fe^{3+}/H^+$  (O) ion-exchange processes.



Fig. 6. The entropy changes of the ion-exchange processes as a function of the crystalline ionic radii.

The change of enthalpy,  $\Delta H^{\circ}$ , of free energy,  $\Delta G^{\circ}$ , of entropy,  $\Delta S^{\circ}$ , and the temperature dependence on  $\ln K$  (Fig. 5), have been calculated and the results are given in Tables IV-VI. Furthermore, Fig. 5 shows that the  $\ln K = f(I/T)$  plot is

linear over a wide range of remperature (25-250°). The exchange reactions are therefore endothermic.

The results obtained in the present study of the  $Eu^{3+}/H^+$  ion-exchange process can be compared with those obtained by BAETSLE<sup>9</sup>. The values of the enthalpy change,  $\Delta H^{\circ}$ , show a notable difference, owing to the method of evaluation of the thermodynamic equilibrium constants.

The dependence of the entropy changes determined for the ion-exchange processes on the crystalline radii of the ions is presented in Fig. 6, and can be seen to be linear. The linear dependence of the entropy change could be explained if it is assumed that the material used in our experiments has a semicrystalline structure. This change of crystalline structure in the amorphous samples treated at higher temperature was observed in our earlier work<sup>14</sup>.

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